A Novel Approach for Dynamics Compensation in Boiler Drum Level Control

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Abstract : The boiler drum level control is one of a critical control in a power generation plant because the fluctuation in the water level will leads to uneconomical situation .In generally large power generation plant has three element control scheme is used for boiler drum level control. Three element control scheme is one of the most control methodology used in a high pressure boilers. In this conventional scheme the boiler drum oscillations, power loss are occurred also the high pressure of water to spoil the control valve life time. This are all the dynamics occurred during the boiler operation it will lead to affect the steam production and boiler performance also affects the overall plant performance. To overcome the drawbacks of existing method of control scheme the implementation of feed water flow pressure compensation method is used to which control valve life time and reduced water fluctuation in the drum. The VFD control is used to achieve the feed water flow pressure compensation. VFD will receive the control signal from PID4 based on the signal the frequency variation will lead to drive the pump. Since the feed water pump is controlled using VFD and the pressure is also compensated and level is maintained properly and fluctuation is also reduced. This project work was implemented a 32MW cogeneration thermal plant with the help of yokogawa DCS.

Keyword : Boiler drum, level, flow, steam, feed water, shrinkage, dynamics, swelling.

1. INTRODUCTION

In thermal Power Station fuel burns & uses the resultant to make the steam, which derives the turbo generator. The Fuel coal is burnt in pulverized from. The pressure energy of the steam produce is converted into mechanical energy with the help of turbine. The mechanical energy is fed to the generator where the magnet rotate inside a set of stator winding & thus electricity is produced in India 65% of total power is generation by thermal power stations.

2. COGENERATION PLANT

This control scheme is implanting a cogeneration plant with a capacity of 25 MW power generations. The plant is operational with Multi Fuel High Pressure Boilers and Turbines.

3. BOILER

Boiler is defined as a closed vessel in which steam is produced from water by the combustion of fuel. Generally, in boilers steam is produced by the interaction of hot flue gases with water pipes which is coming out from the fuel mainly coal or coke. In boilers, chemical energy of stored fuel is converted into the heat energy and this heat energy is absorbed by the water which converts them into a steam. Boilers have many serious injuries and destruction of property. It is critical for the safe operation of the boiler and

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the steam turbine. Too low a level may overheat boiler tubes and damage them. Too high a level may interfere with separating moisture from steam and transfers moisture into the turbine, which reduces the boiler efficiency. Various controlling mechanism are used to control the boiler system so that it works properly.

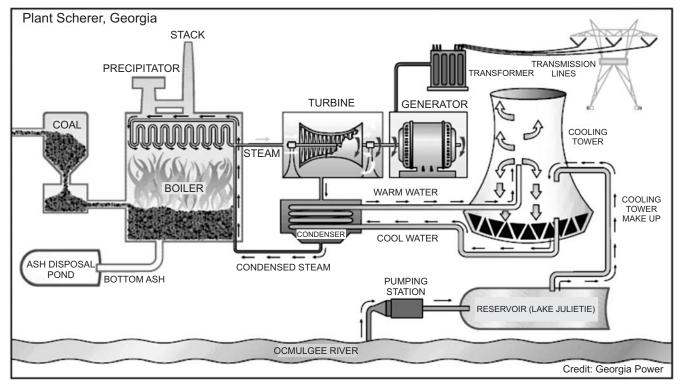


Figure 1: Layout of Cogeneration Plant

3.1. Water Tube Boiler

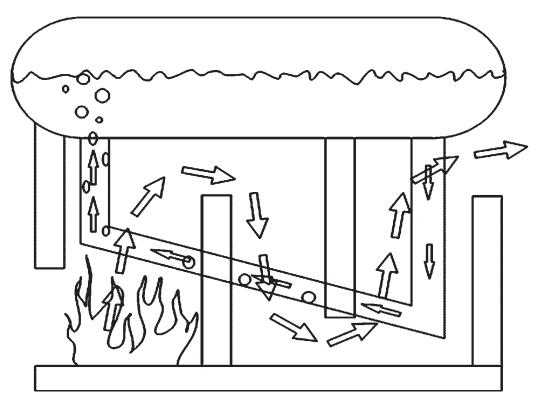


Figure 2: Water tube boiler

A Water tube boiler is a type of boiler in which water circulates in tubes heated externally by the fire. Fuel is burned inside the furnace, creating hot gas which heats water in the steam-generating tubes. In smaller boilers, additional generating tubes are separate in the furnace, while larger utility boilers rely on the water-filled tubes that make up the walls of the furnace to generate steam. The heated water then rises into the steam drum. Here, saturated steam is drawn off the top of the drum. In some services, the steam will reenter the furnace through a superheated to become superheated. Superheated steam is defined as steam that is heated above the boiling point at a given pressure. Superheated steam is a dry gas and therefore used to drive turbines, since water droplets can severely damage turbine blades.

3.2. Necessity of Level Maintenance

The drum level must be controlled to the limits specified by the boiler manufacturer. If the drum level does not stay within these limits, there may be water carryover. If the level exceeds the limits, boiler water carryover into the super-heater or the turbine may cause damage resulting in extensive maintenance costs or outages of either the turbine or the boiler. If the level is low, overheating of the water wall tubes may cause tube ruptures and serious accidents, resulting in expensive repairs, downtime, and injury or death to personnel. A rupture or crack most commonly occurs where the tubes connect to the drum.

3.3. Swell & Shrink

Under steady-state conditions, both water and steam bubbles reside below the water surface. The average mixture density is constant. Should steam demand increase, the steam bubbles expand under the water surface, increasing the average mixture density. This causes an increase in steam drum level without the addition of feed water. This increase in level proportional to an increased steaming rate and decreased drum pressure is called swell.

Inversely, as the steam load decreases, the steam bubbles in the steam/water mixture decrease in size and volume. This causes a decrease in drum level, although the mass of water and steam has not changed. This phenomenon is called shrink.

3.4. Boiler Drum Level Control

The drum level must be controlled to the limits specified by the boiler manufacturer. If the drum level does not stay within these limits, there may be water carryover. If the level exceeds the limits, boiler water carryover into the super-heater or the turbine may cause damage resulting in extensive maintenance costs or outages of either the turbine or the boiler. If the level is low, overheating of the water wall tubes may cause tube ruptures and serious accidents, resulting in expensive repairs, downtime, and injury or death to personnel. A rupture or crack most commonly occurs where the tubes connect to the drum. Damage may be a result of numerous or repeated low drum level conditions where the water level is below the tube entry into the drum. When the drum level gets too low, the boiler must have a boiler trip interlock to prevent damage to the tubes and cracks in the tubes where they connect to the boiler drum. The water tubes may crack or break where they connect to the drum, or the tubes may rupture resulting in an explosion. The water tube damage may also result in water leakage and create problems with the drum level control. The water leakage will affect the drum level because not all the water going into the drum is producing steam. Poor level control also has an effect on drum pressure control. The feed water going into the drum is not as hot as the water in the drum. Adding feed water too fast will result in a cooling effect in the boiler drum reducing drum pressure and causing boiler level shrinkage.

3.5. Boiler Drum Level Control System

- 1. Single element drums level (feedback) control
- 2. Two element drum level (feedback and feed forward) control
- 3. Three element drum level (cascade) control

3.5.1. Three Element Drum Level Control

This control system is ideally suited where a boiler plant consists of multiple boilers and multiple feed water pumps or feed water valve has variation in pressure or flow. It requires the measurement of drum level, steam flow rate, feed water flow rate and feed water control valve. By using cascade control mechanism level element act as a primary loop and flow element act as a secondary loop and steam flow element act as a feed forward controller. Level element and steam flow element mainly correct for unmeasured disturbances within the 7 system such as boiler blow down. Feed water flow element responds rapidly to variations in feed water demand either from the feed water pressure and steam flow rate of feed forward signal. The performance of the three-element control system during transient conditions makes it very useful for general industrial and utility boiler applications. It handles loads exhibiting wide and rapid rates of change.

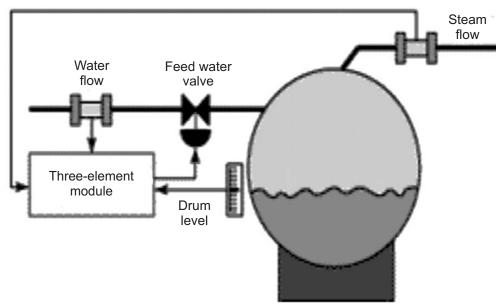


Figure 3: Three elements drum level control

3.5.2. Three Element Feed Control System

The feed water control system is a three element type, designed to monitor changes in steam flow, water flow and drum level. Steam flow is the rate of steam leaving the boiler- the demand. Water flow is the rate of feed water flow into the boiler - the supply. Drum level reflects the amount of water in the boiler - the inventory. With changes in boiler load (steam flow), steam and water flow become unbalanced and water level consequently deviates from the normal position. In such an event, the system changes water flow to the extent necessary to restore the balance between steam flow and feed flow and return the water level to normal.

4. OUTDATED SYSTEM

Existing Method

This control system is ideally suited where a boiler plant consists of multiple boilers and multiple feed water pumps or feed water valve has variation in pressure or flow. It requires the measurement of drum level, steam flow rate, feed water flow rate and feed water control valve. By using cascade control mechanism level element act as a primary loop and flow element act as a secondary loop and steam flow element act as a feed forward controller. The performance of the three-element control system during transient conditions makes it very useful for general industrial and utility boiler applications. It handles loads exhibiting wide and rapid rates of change. Figure depicts the control scheme for three-element drum level control. These are P for the proportional term, I for the integral term and D for the derivative term in the controller. Threeterm or PID controllers are probably the most widely used industrial controller. Even complex industrial control systems may comprise a control network whose main control building block is a PID control module. The PID controllers separately calculate the three parameters. The proportional, the integral, the derivative values. The proportional value determines the reaction to the current error. The integral value determines the reaction based on the sum of recent errors as past error. The derivative value determines the reaction based on the rate at which the error has been changing as a future error. And the 100% control valve are maintained the drum level. So the draw backs like fluctuation and power loss which affects the overall efficiency.

Control scheme

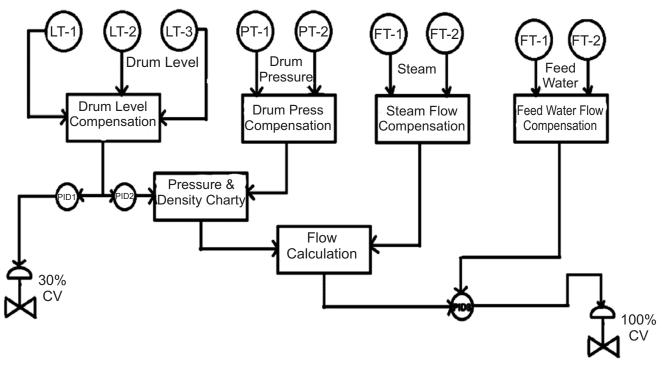


Figure 4

Three parameters are measured like drum pressure, steam flow and feed water flow. Drum level value is measured and then given to the PID 1 and PID2. PID2 is used to control the 30% control valve which is only used for emergency condition and also as single element controller to control level. When we use the 30% control valve we can only generate 10MW of the total 25MW power production capacity, so we always go for 100% control valve Pressure in the boiler drum is measured by the differential pressure transmitter and the value is given to the pressure and density charity. Pressure value is measured and the density can be found out using the pressure and density charity. PID1 controller output is also given to the pressure and density charity, flow is calculated using the calculating function. Calculated flow value is then given to the PID3 and also feed water flow .PID3 value is given directly to the 100% control valve. Where the Controllers PID1,PID2,PID3 were implemented in a plant with help of Yokogawa DCS centum 3000, all the controllers minimum value of Derivative has been chosen.

Flow calculation

Compensation Flow = Q* Current Flow $Q = \sqrt{(\text{Desired Temp * Actual Pressure)} / (\text{Desired Pressure * Actual Temp})}$

Table 1					
Drum Pressure	Water Density	Steam density			
0	1	0			
45.04	0.791	0.217			
61.6899	0.75	0.025			
71.57	0.741	0.0305			
76.94	0.7322	0.03607			
82.62	0.725	0.0395			
88.64	0.741	0.0425			
101	0.66	0.0522			

Pressure and Density Charity

Drawback of existing scheme

Three element control scheme is one of most control methodology used in a High pressure boilers. Even though the power loss, drum oscillation and high pressure water to spoil the life control valve life time. This dynamics are occurred during the boiler operation it will lead to affect the steam production and boiler performance also affects the coverall plant performance.

5. PROPOSAL SYSTEM

To overcome the drawbacks of existing method of control scheme the implementation of feed water flow pressure compensation method is used to which control the water level in boiler drum and overcome the dynamics. Like power loss is reduced, increase the control valve life time and reduced water fluctuation in the drum. The VFD control is used to achieve the feed water flow pressure compensation. VFD will receive the control signal from PID4 based on the signal the frequency variation will leads to drive the pump. Since the feed water pump is controlled using VFD and the pressure is also compensated and level is maintained properly and fluctuation is also reduced.

Control scheme of proposed system

Three element drum level control is used for the control of water level in boiler drum. Three parameters are measured like drum pressure, steam flow and feed water flow and there dynamics are reduced. Drum level value is measured and then given to the PID 1 and PID2. PID2 is used to control the 30% control valve which is only used for emergency condition and also as single element controller to control level. When we use the 30% control valve we can only generate 10MW of the total 25MW power production capacity, so we always go for 100% control valve .Pressure in the boiler drum is measured by the differential pressure transmitter and the value is given to the pressure and density charity. Pressure value is measured and the density can be found out using the pressure and density charity. PID1 controller output is also given to the pressure and density charity to the drum pressure value. According to the steam flow and density charity, flow is calculated using the calculating function. Calculated flow value is then given to the PID3 and also feed water flow. PID3 value is spitted into two. One is given directly to the 100% control valve and another one is PID4 which has the same characteristics as PID3. A constant pressure is compensated to the PID4 because the pressure of the feed water flowing in the pipes should be more than the boiler drum pressure. If it is less means the water will not flow so we are compensating a constant pressure. Now the PID4 control value is given to the Variable frequency drive. VFD will control the feed water pump and level is being maintained. It can eliminate the more fluctuation in the boiler drum level and save the power loss. According to the characteristics of pump, it can be found that the flux varies due to different motor speed. On condition that less water is needed in operation, we can decrease the motor speed through the VFD rather than the valve, we can save a lot electricity.

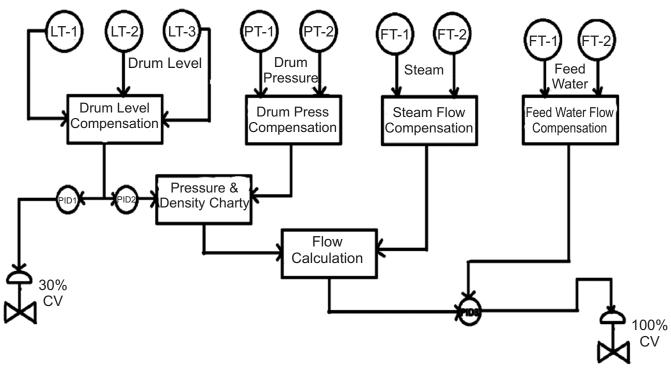


Figure 5: Control scheme of proposed system

6. VARIABLE FREQUENCY DRIVE (VFD)

Boiler Feed Water Pump Controls

Boiler feed water systems are critical to overall power plant performance, but can be one of the single largest energy consumers in the plant. As electrical demand fluctuates, the required boiler feed water flow rate changes to match make-up water demand. Feed water flow is created by a large pump that operates at full speed and a modulating valve opens and closes to vary the flow rate supplied to the boiler. This boiler feed water system consisting of a modulating throttle valve to control flow rate is effective but requires frequent valve maintenance and wastes energy.

A Better Way

Reduce energy consumption and lower maintenance cost by controlling boiler feed water flow with a variable speed drive rather than a throttling valve. Boiler feed water flow can be controlled by varying the speed of the electric motor that controls the speed of the pump and modulates the water flow to the boiler. By controlling flow using a variable speed drive, the electric motor uses much less horsepower and there for less kilowatts as compared to the throttling valve. In this new control scenario, the feed water valve should be 100% open or removed so to not restrict water flow. Since the throttle valve is no longer being operated, there is reduced valve maintenance cost. For example, the boiler feed water pump operating at 20% less flow (the pump operates 20% slower), can result in a 50% reduction in energy savings (based on the Affine nifty Laws).

Pump Flow Control

On large pumps, significant energy savings can be realized by replacing a fixed speed motor and old flow control technology with a variable speed motor. This example is a pump supplying water to a process and driven by a fixed speed induction motor. The water flow is controlled with a diaphragm operated control

valve controlled by a signal from the process control system (PLC or DCS). If less flow is required the valve is partially closed, which reduces the flow to the desired value and increases the pump pressure at the same pump speed. This is called flow throttling, and the pressure drop across the valve causes energy to be lost. Also since the pump is working against a higher pressure, more energy is required from the motor. The situation is much improved if a variable speed motor, supplied by a variable frequency drive (VFD), is used. The control valve is no longer required since the flow is varied by changing the motor speed. The VFD is supplied by 50 or 60 Hertz three-phase power, and creates a three-phase output of any desired frequency. The motor changes speed to match the frequency supplied to it, and drives the pump at this speed, which produces the desired flow. To reduce the flow there is no throttling and the pump supplies the flow against a much lower pressure, so the motor power required is much less. This represents a significant energy savings, especially if the reduced flow continues for any extended period.

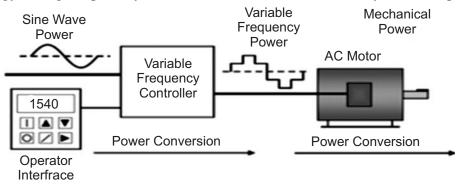


Figure 5: Working of VFD

Variable Frequency Drive in Thermal Power Plant

The application of the medium voltage variable frequency drive in the large-sized asynchronous motor is just at the initial stage in China, which, however, has been pretty popular in the developed countries.

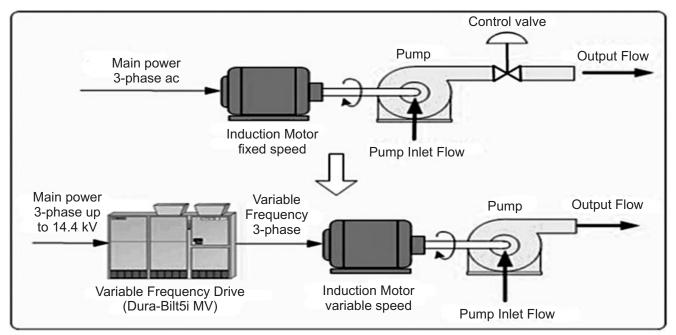


Figure 6: Pump flow control

As the development of the electronic components, types of the medium voltage VFD become very diverse. By the topological structure, the medium voltage VFD can be classified as IGBT module serial-connection type, tri-level type and multiple power unit serial-connection type with voltage superposition.

Considering that there will be just a little pressure change, we decided to only reconstruct the 2# water supply pump with the variable frequency drive.

Adopt the mode of one VFD to control one pump, and no need to add power frequency bypass system.

Take 4~20mA current of the pressure transmitter from the pumping main as the feedback signal, and obtain the given frequency from the DCS system.

Run signal and stop signal are given by the DCS system.

The condition signal of the medium voltage VFD is sent from the control cabinet to the DCS system for the purpose of instantaneous detection.

The pressure value of the pumping main can reach or overrun the requested 6.8MPa after reconstruction.

Shut down the by-pass value of each pump, and the appropriate flux can be produced by adjusting the speed of the motor through the medium voltage VFD.

Close-Loop\Control

Shut down the by-pass valve of each pump, and realize close-loop control by the VFDs PID function, and the DCS system will provide the given 4~20mA corresponding to 0~10MP. And the press transformer on the pumping main will feed back the 0~10MP press signal to the VFD, and to control output torque by PID, so as to adjust the water flux.

VFD Control

A VFD controls the speed of an ac motor, which provides flexibility to the process since speed can be changed easily for process optimization. It takes the fixed power supplied to it and converts it into a variable frequency and variable voltage source which then feeds a motor. This allows the drive to control the speed and torque the motor produces.

A VFD may enhance the user's profitability by improving the process.

7. SIMULATION WORK

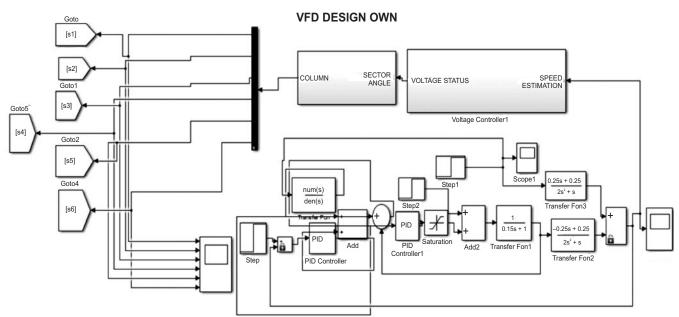


Figure 7: VFD Using PID Controller

The transfer function and PID controller Values are collected from the plant and same values has been chosen. The proposed system has been simulated in the matlab in the fig 7. In the three element boiler drum level control the parameters are like level, steam flow and water flow. The feed forward disturbance is steam flow and the cascade is level and feed water flow. Level, water flow, steam flow and control value

has been implemented using the transfer functions. Proportional, integral and derivative gain has been derived using the Ziegler-Nicholas method and implemented in respective PID controller. Set point for level has been set initially and the output can be seen through Scope 1.

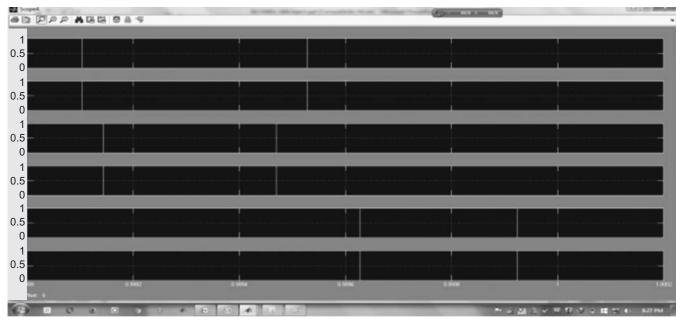


Figure 8: Response for the variable frequency power

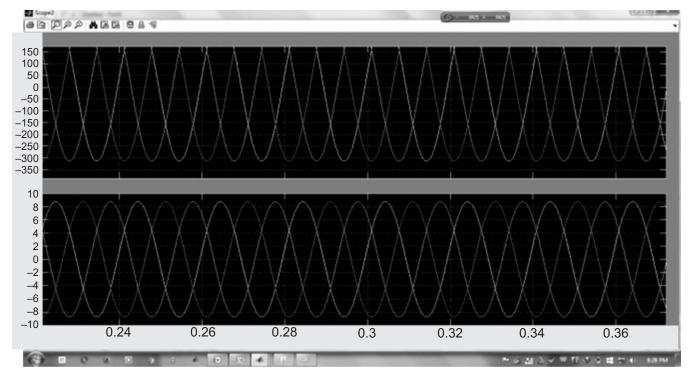


Figure 9: Three phrase ac current and voltage

The scope value is split and then given to the Control limiter which performs the function of limiting the value within a specified limit. From there to the PWM generator and the respective angle will be chosen and which in turn triggers the Mosfet. AC three phase current to the mosfet to trigger on the gate open and close are depend on the PWM. AC is converted to DC using rectifier .Again Dc is converted using inverter into AC .AC signal is then given to the filter to reduced the noise and give the clear sine wave to run the asynchronous motor and the hydraulic pump. Using scope2 we can view the drum level and water flow rate.

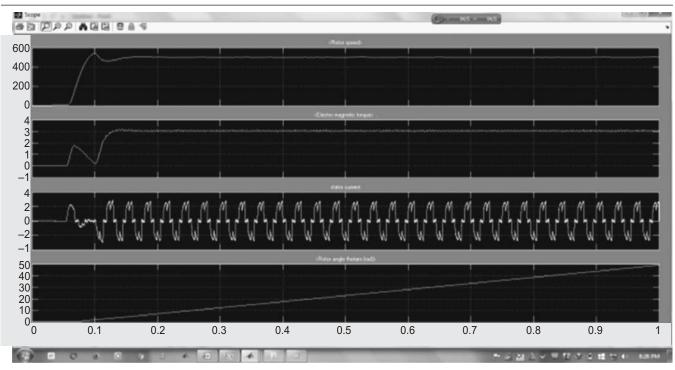


Figure 10: Rotor speed, torque, stator current and rotor angle

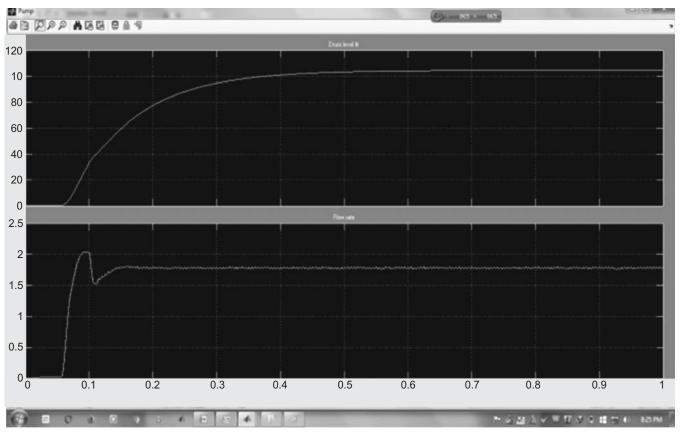


Figure 11: Response for drum level control and feed water flow

8. RESULT

The performance of VFD based controllers are evaluated using the considered groups of system and their. comparative responses are shown in Figure 7.5. From the graphs above we can calculate the rise time along with settling time and steady state.

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Table 2 Time Domain Specification for Three Element Drum Level Control with VFD Using PID Controller

S. No.	Rise Time(tr)(sec)	Settling Time(ts)(sec)	Over shoot (%) (Mp)	Peak(tp) (sec)
01	0.49	1.6	0.13	0.7

The delay time is to **be** *td* : **0.05sec** and time constant **tc** : **0.16sec**. In a boiler drum level the dynamics are like Integrating process, Inverse response, swelling, shrinkage. Due to this only the inlet flow of feed water pressure has to be compensated. So the time constant and delay time will not affect the performance of boiler.

Table 3Level and Feed Water Flow

S. No.	Level (cm)	Flow Rate (LPH)	Speed (rpm)	Frequency (Hz)
01	200	216	1000	16.7
02	350	360	1760	29.5

Process Variable (PV) : Level

Set point SP	:	110M
Delay time td	:	0.05s
Rise time tr	:	0.26s
Time Constant tc		0.16s
Settling time ts	:	0.5s

The control objective is regulating the pressure of feed water inlet flow to the boiler drum is to be compensated by using VFD. The VFD operate the pump at different speed, the variation in pump speed can be achieved in pressure of water flow can be achieved. So we can obtain the compensated pressure flow of feed water it should overcome the effects of boiler.

9. CONCLUSION

A novel approach for a better control of drum level using a VFD. A simple VFD control is implemented and the corresponding results were studied. Thus by maintaining the drum level using VFD, we reduce the fluctuation in boiler drum, save power and increase the life of the control valve. Therefore overall efficiency of the process increases.

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